

**RECEIVED  
CENTRAL FAX CENTER****MAY 27 2008****Amendments to the Specification:**

On page 6, please replace the second paragraph starting on line 2, with the following amended paragraph:

The hydrocarbon mixture for reforming is fed via the valve 16 and the filter 15 to the pump 2. The pressure downstream of the pumps is maintained within the limits 2.0 to 2.5 MPa. The pressure gauge 14, the thermometer 13 and flowmeter ~~[[15]]~~ 12 monitor the pressure, the temperature and the flow rate, respectively, of the raw petrol at the working segment from the delivery pump 2 fo the horizontal vacuum chamber 1. At the startup of the plant operation valves 16, 17 and 18 are open. The required evacuation in the vacuum chamber is monitored with the vacuum gauge 11 connected to the front part of the vacuum chamber.

On page 7, please replace the second paragraph starting on line 4, with the following amended paragraph:

This pressure has been found to constitute: for raw petrol processing, 1 to 12 MPa; for fuel oil processing, 10 to 12 MPa; for diesel oil processing, 5 to 6 MPa; for crude oil processing, 4 to 7 MPa.

On page 7, please replace the fourth paragraph 4 starting on line 11, with the following amended paragraph:

The average integral value of saturation pressure of the produced low-boiling mixture component, e.g. of refined petrol, varies within the limits of 0.005 to [[0.7]] 0.07 MPa and is equal to its saturation pressure at the temperatures 4 to 80 °C, which entails originating of a gas phase in the jet lift-off area.

On page 7, please replace the second to the last paragraph starting on line 21, with the following amended paragraph:

This results in formation of an emulsion with gas bubbles of [[5]] 0.5 to 7  $\mu\text{m}$  size, which essentially creates the second phase of the working medium.